

Effect of Carbon-based Additives on Hydrogen Production in the Air/Steam Gasification of Dried Sewage Sludge

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Introduction

- This paper discusses the challenges associated with sewage sludge disposal and the potential of thermochemical conversion, specifically gasification, as a sustainable and efficient disposal method.
- The addition of air and steam mixtures to gasification has been shown to be an economically viable method.
- Carbon materials, such as activated carbon, bio char and lignin char, have also been identified as potential catalysts for gasification.
- However, the poor physicochemical properties of raw biochar and the tendency of catalysts to coke and sinter on the biochar surface limit their effectiveness.
- Despite these limitations, the presence of inherent alkali and alkaline earth metals (AAEMs) in biochar makes them effective as catalyst supports for tar cracking/reforming and enhancing the water gas shift reaction in gasification applications.
- The article also highlights the water-gas shift and steam methane reforming reaction

Materials and Methods

Feedstock and catalyst

- Feedstock: Sewage sludge (SWS) was obtained from a wastewater treatment facility in South Korea and dried at 110 °C in oven for 24 h to obtain dried sewage sludge (DSS).

- Physicochemical properties of DSS, AC, bio char and Lignin char

Proximate analysis (%)	DSS	Activated carbon	Bio char	Lignin char
Moisture	2.5	1.15	0.67	0.85
Volatile matter	56.8	8.26	24.18	36.4
Ash	40.7	11.19	75	28.81
Fixed carbon	-	79.39	0.14	33.94

Ultimate analysis (%)	DSS	Activated carbon	Bio char	Lignin char
C	49.3	83.77	77.28	63.69
H	5.1	0.57	2.65	1.16
N	5.3	0.27	0.69	0.8
O	39.5	15.13	19.38	32.6
S	0.9	0.26	-	1.75

Catalyst analysis

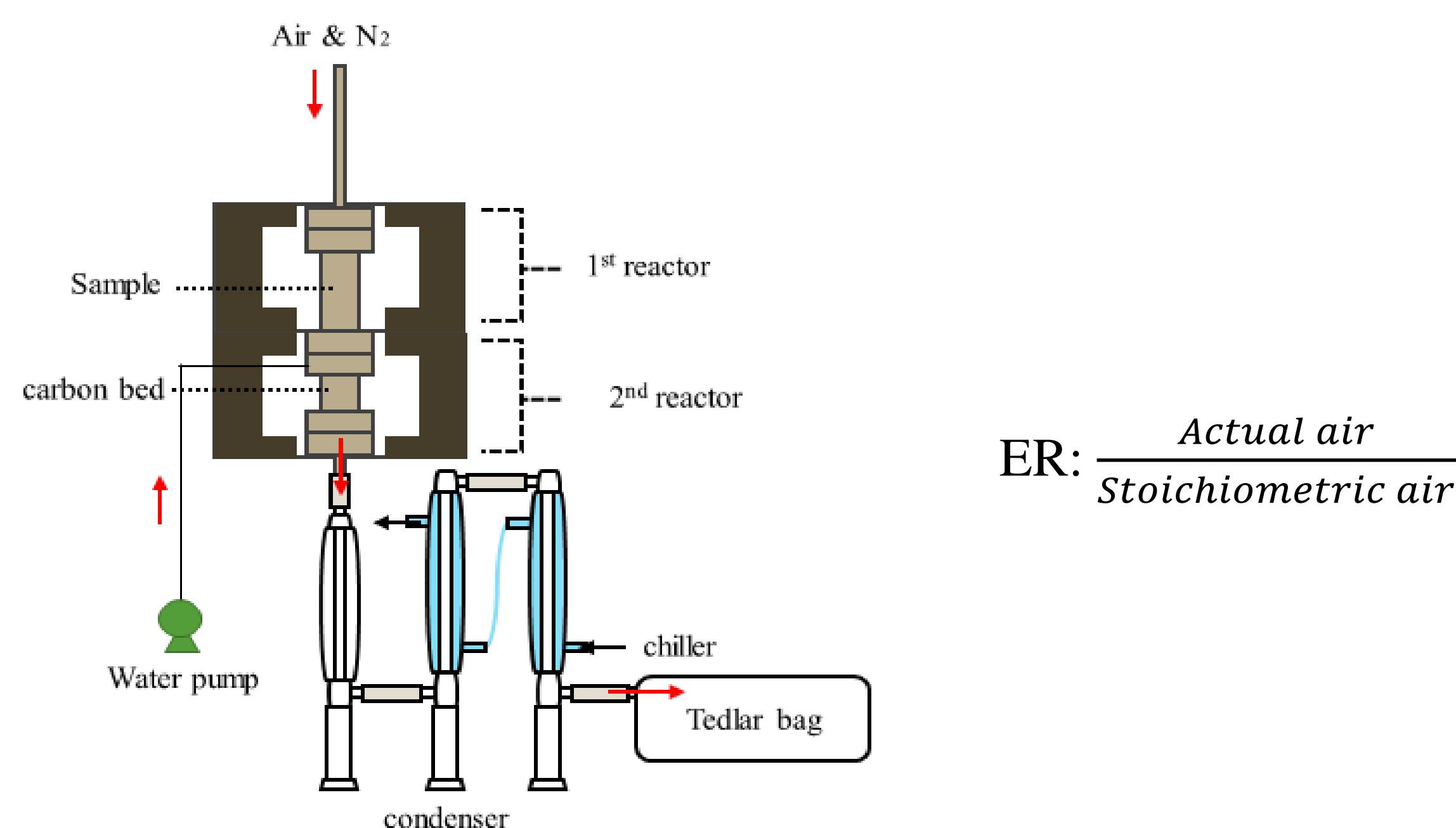
- BET analysis
 - The physical characteristics of carbon based additives were determined using BET analysis on surface area and a porosity analyzer (3Flex, version 3.02, Micrometrics, USA).
 - 0.3 mg of each catalyst was first preheated at 180 °C for 8h in a vacuum by N₂ adsorption-desorption at -196 °C.

Gasification experiment

- Parameters for gasification experiments for all runs

	Non catalytic	Activated carbon			Bio char			Lignin char		
		R2	R3	R4	R6	R7	R8	R9	R10	
Reaction number	R1	R2	R3	R4	R5	R6	R7	R8	R9	R10
Catalyst Bed Temperature	-	750	800	850	750	800	850	750	800	850
Steam(ml)	-	5	10	15	5	10	15	5	10	15
ER	-	0.2								

- Schematic setup for the catalytic gasification dried sewage sludge (DSS) using air and air with steam.

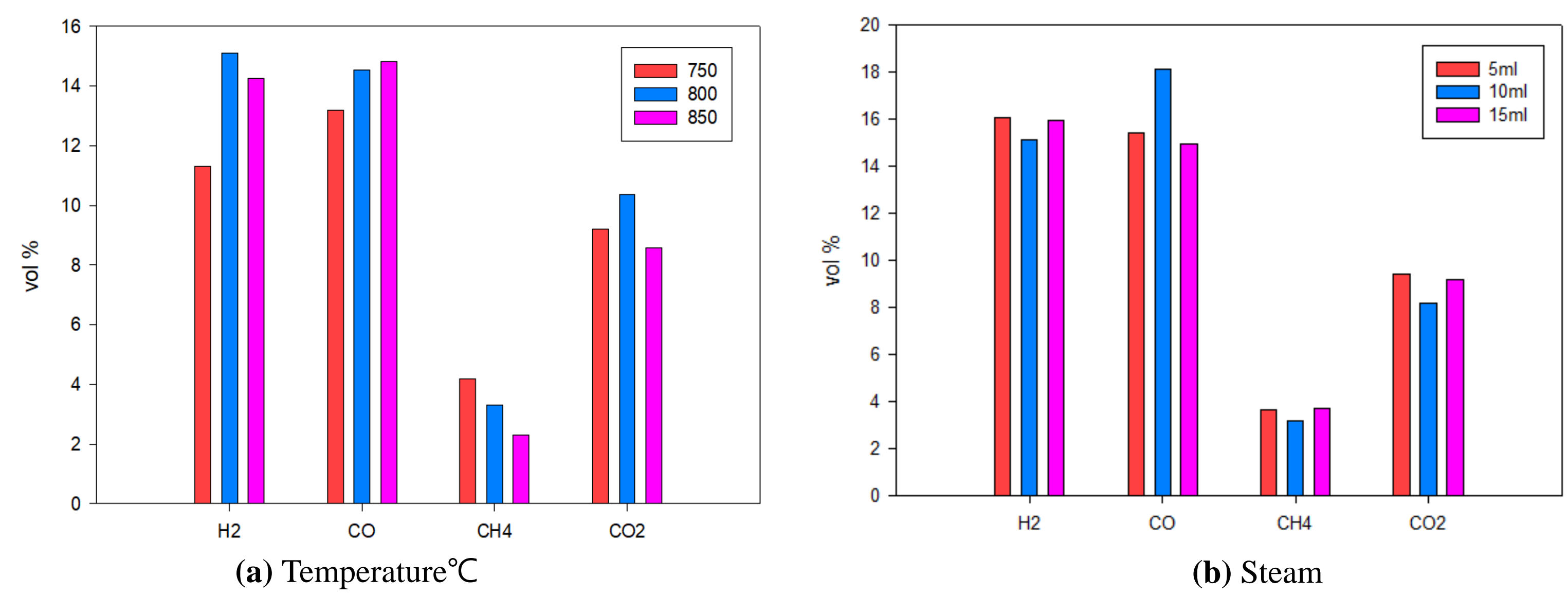


Results

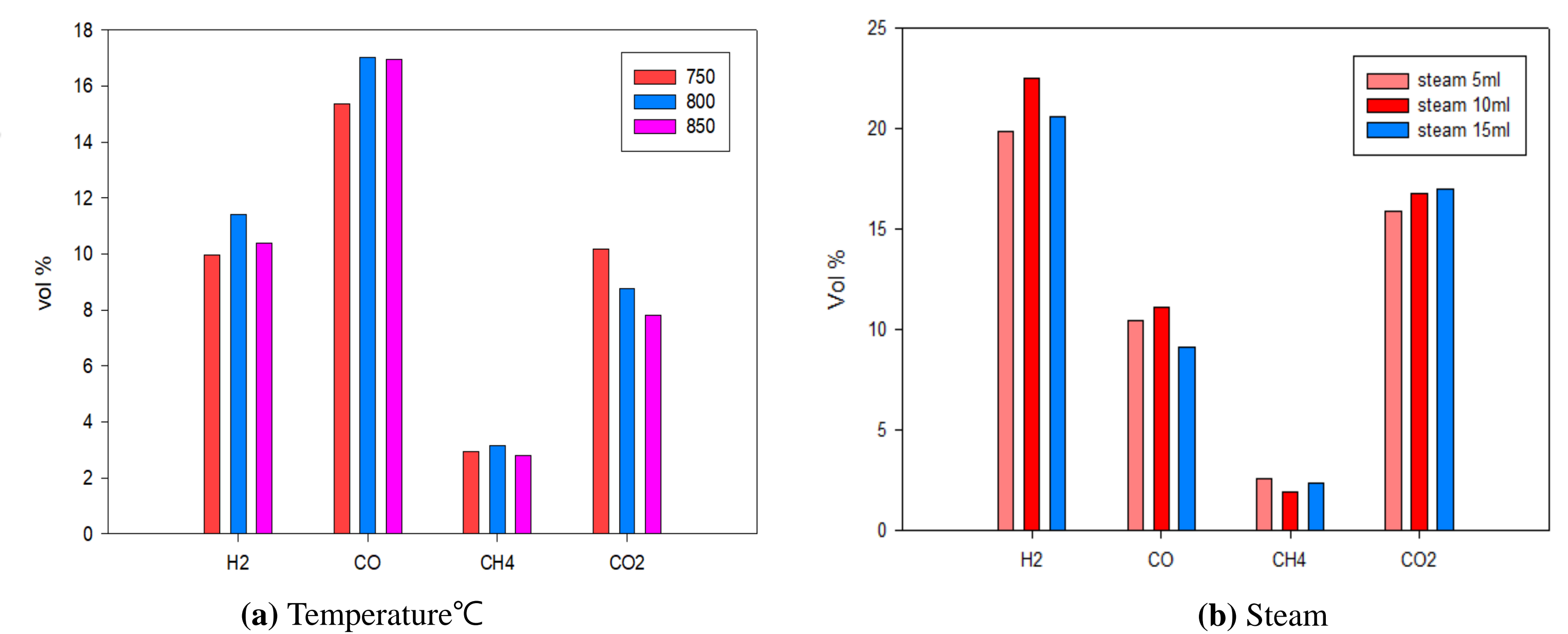
Physical characteristics of the catalysts in this study

Catalyst	Surface area (m ² /g)	Total pore volume (cm ³ /g)
Activated carbon	1043.31	0.519
biochar	14.05	0.012
lignin char	3.28	0.007

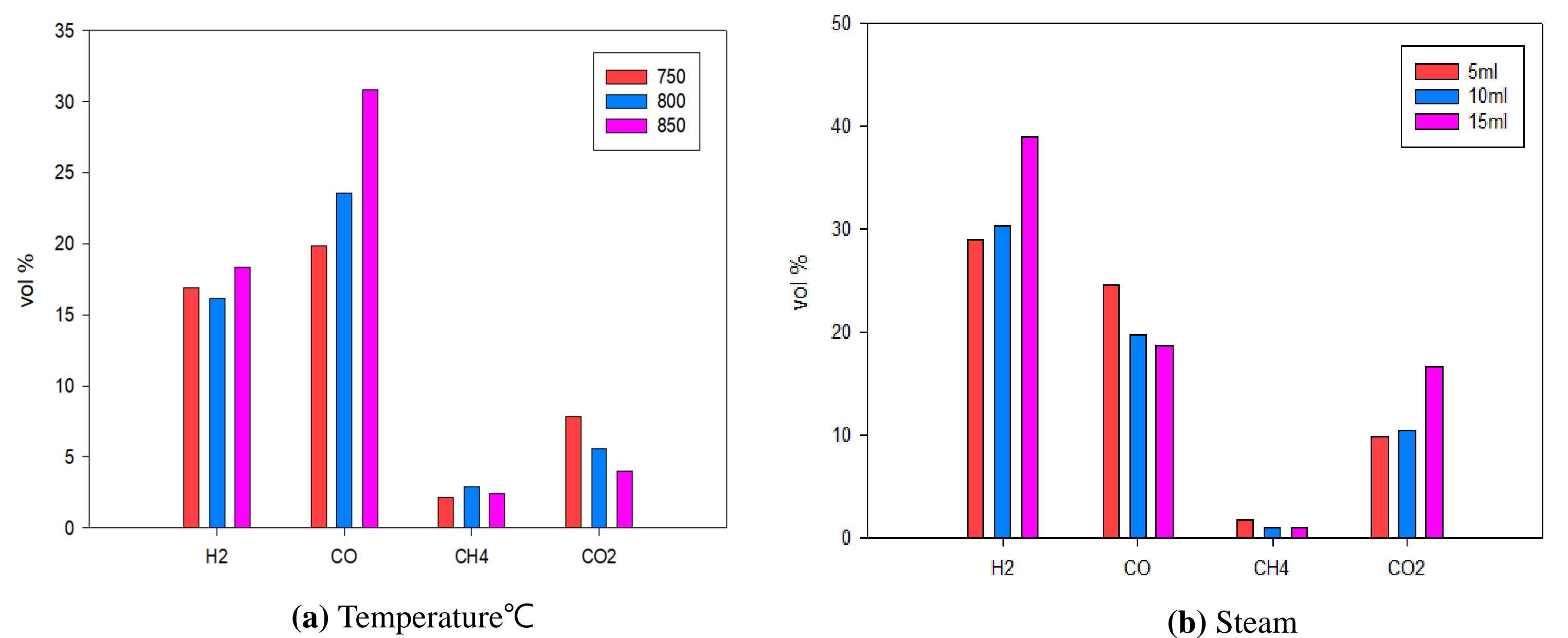
Effect of air/steam injection and reaction temperature on gas selectivity of DSS gasification(Activated carbon)



Effect of air/steam injection and reaction temperature on gas selectivity of DSS gasification(Bio char)



Effect of air/steam injection and reaction temperature on gas selectivity of DSS gasification(Lignin char)



Conclusions

- The carbon based additives particle size of 0.5 mm–1.7 mm and temperature of 800 °C showed optimum results in terms of higher gas yield, high H₂ and low CO₂ in the product gas when air was used as the gasifying agent.
- The induction of steam only showed a positive effect in the case of biochar and lignin char because the water-gas shift reaction and hydrocarbon reforming, resulting in a higher H₂ selectivity of ~35vol%.
- It can be concluded that the presence of AAEMs in biochar is more efficient for higher H₂ generation via an enhanced water-gas shift reaction than the higher surface area of activated carbon with no AAEMs.
- This study provides an excellent and sustainable solution for enhancing H₂ generation using activated carbon and low-cost biochar and lignin char catalysts under different gasification conditions.

Acknowledgement

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